AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions, and listings, of claims in the application:

1. (Currently Amended) An alkaline peroxide mechanical pulping process comprising the steps of:

feeding a lignocellulosic material into a first press;

pressing the lignocellulosic material;

discharging the lignocellulosic material from the first press;

impregnating the lignocellulosic material discharged from the first press with a first <u>sodium hydroxide</u> alkaline peroxide pretreatment solution and maintaining the impregnation for a first reaction time;

feeding the impregnated lignocellulosic material to a refiner having an inlet and a rotating disc within a superatmospheric casing;

refining the impregnated lignocellulosic material to form a primary pulp having a temperature of at least about 80C;

delivering a stream of primary pulp from the superatmospheric casing to an intermediate a blow line while the primary pulp temperature is at least about 80C;

adding an <u>a sodium hydroxide</u> alkaline peroxide intermediate <u>blow</u> line solution to the stream of primary pulp within the intermediate in the blow line while the primary pulp temperature is at least about 80C:

mixing the intermediate blow line solution and the stream of primary pulp to form a reaction mixture in the intermediate blow line;

discharging the reaction mixture having a temperature of at least about 80C into a retention vessel;

retaining the reaction mixture in the retention vessel to produce a bleached material.

2. (Currently Amendment) The alkaline peroxide mechanical pulping process of claim 1 further comprising;

feeding the lignocellulosic material that has been impregnated with the first pretreatment solution for a first reaction time, into a second press;

pressing and discharging the lignocellulosic material from the second press;

impregnating the lignocellulosic material discharged from the second press with a second <u>sodium hydroxide</u> alkaline peroxide pretreatment solution and maintaining the second impregnation for a second reaction time.

- 3. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 1 further comprising adding an <u>a sodium hydroxide</u> alkaline peroxide refiner solution to the lignocellulosic material at the refiner.
- 4. (Original) The alkaline peroxide mechanical pulping process of claim 1, wherein the step of feeding the impregnated lignocellulosic material to a refiner having an inlet and a rotating disc within a superatmospheric casing includes maintaining the superatmospheric casing at a pressure of at least about 240kPa.
- 5. (Original) The alkaline peroxide mechanical pulping process of claim 1, wherein the step of mixing is immediately followed by introducing the mixture into a separator and the separated pulp is then discharged into said retention vessel.
- 6. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 1, wherein the step of adding an alkaline peroxide intermediate blow line solution to the stream of primary pulp within the intermediate line includes adding the intermediate blow line solution immediately after a the blow valve.
- 7. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 5, wherein the step of adding an alkaline peroxide intermediate blow line solution to the stream of primary pulp within the intermediate line includes adding the intermediate blow line solution immediately prior to the separator.

- 8. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 1, wherein the step of delivering a stream of primary pulp from the superatmospheric casing to a intermediate the blow line further includes the primary pulp having a temperature in the range of about 90C to about 155C and a consistency of about 20 to about 60%.
- 9. (Original) The alkaline peroxide mechanical pulping process of claim 1, wherein the reaction mixture is retained in the retention vessel at a temperature of about 60C to about 95C and a consistency of about 20% to about 40%.
- 10. (Original) The alkaline peroxide mechanical pulping process of claim 1, wherein the reaction mixture is retained in the retention vessel at a temperature of about 85C to about 95C, and a consistency of about 30%.
- 11. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 1, wherein the impregnation solution contains alkali sodium hydroxide, peroxide, and stabilizer; the intermediate blow line solution contains alkali sodium hydroxide, peroxide, and stabilizer; and said intermediate blow line solution has a temperature less than about 80C.
- 12. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 2, wherein the first impregnation solution contains 0.3% DTPA; the second impregnation solution contains by weight per cent 0.2% MgSO4, 4.4% silicate, 2.8% TA, and 2.8%H2O2; and the intermediate blow line solution contains by weight per cent 0.16% DTPA, 0.16% MgSO4, 2.3% silicate, 1.8% TA with 0.5% being residual, 2.4% H2O2 with 1.1% being residual.
- 13. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 2, wherein the first impregnation solution contains by weight per cent 0.5% DTPA; the second impregnation solution contains by weight per cent 0.2% DTPA, 0.1% MgSO4, 2.0% silicate, 1.6% TA, and 2.6%H2O2; and the intermediate blow line solution

contains by weight per cent 0.13% DTPA, 0.13% MgSO4, 2.5% silicate, 1.2% TA with 0.1% being residual, 2.1% H2O2 with 2.1% being residual.

- 14. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 2, wherein the first impregnation solution contains by weight per cent 0.3% DTPA, 0.05% MgSO4, 0.7% silicate, 0.2% TA, and 0.5%H2O2; the second impregnation solution contains by weight per cent 0.1% DTPA, 0.08% MgSO4, 1.8% silicate, 1.4% TA, and 1.9%H2O2; and the intermediate blow line solution contains by weight per cent 0.22% DTPA, 0.11% MgSO4, 1.1% silicate, 0.9% TA with 0.2% being residual, 1.2% H2O2 with 1.7% being residual.
- 15. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 2, wherein the first impregnation solution contains by weight per cent 0.4% TA, 0.5% H2O2,0.2% DTPA, 0.04% MgSO4, 0.5% silicate; the second impregnation solution contains by weight per cent 0.14% DTPA, 0.05% MgSO4, 0.5% silicate, 0.4% TA, and 0.6%H2O2; and the intermediate blow line solution contains by weight per cent 0.18% DTPA, 0.06% MgSO4, 1.8% silicate, 1.2% TA with 0.1% being residual, 1.8% H2O2 with 1.1% being residual.
- 16. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 2, wherein the first impregnation solution contains by weight per cent 0.4% TA, 0.6% H2O2,0.18% DTPA, 0.03% MgSO4, 0.3% silicate; the second impregnation solution contains by weight per cent 0.15% DTPA, 0.05% MgSO4, 0.4% silicate, 0.4% TA, and 0.7%H2O2; and the intermediate blow line solution contains by weight per cent 1.7% TA, and 2.8% H2O2 with 1.1% being residual.

17. (Cancelled)

18. (Currently Amended) An alkaline peroxide mechanical pulping process comprising the steps of:

in a primary refiner having a superatmospheric casing, refining a lignocellulosic

material that has been pretreated and impregnated with at least a first <u>sodium hydroxide</u> alkaline peroxide pretreatment solution;

discharging the lignocellulosic material at temperature of at least about 80C into intermediate a blow line having at least one solution inlet port;

injecting an a sodium hydroxide alkaline peroxide intermediate blow line solution through the at least one solution inlet port;

mixing the intermediate <u>blow</u> line solution and the lignocellulosic material in the intermediate <u>blow</u> line;

discharging the lignocellulosic material from the intermediate blow line at a temperature of at least about 80C; and

maintaining the discharged lignocellulosic material for a reaction period.

- 19. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 18, wherein the step of refining further includes adding a refiner solution of <u>sodium</u> <u>hydroxide</u> alkaline peroxide at the primary refiner.
- 20. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 18, wherein the step of injecting an alkaline peroxide intermediate blow line solution through the at least one solution inlet port and into the intermediate blow line containing the lignocellulosic material includes injecting an alkaline peroxide intermediate line solution through, at least, one solution inlet port located immediately within three feet after the blow valve.
- 21. (Currently Amended) An alkaline peroxide mechanical pulping process comprising the steps of:

feeding a lignocellulosic material into a first press;

pressing the lignocellulosic material;

discharging the lignocellulosic material from the first press;

impregnating the lignocellulosic material discharged from the first press with a first sodium hydroxide alkaline peroxide pretreatment solution and maintaining the impregnation for a first reaction time;

feeding the impregnated lignocellulosic material to a refiner having an inlet and a rotating disc within a superatmospheric casing;

refining the impregnated lignocellulosic material to form a primary pulp;

discharging the stream of primary pulp from the superatmospheric casing to an intermediate a blow line;

adding an <u>a sodium hydroxide</u> alkaline peroxide intermediate <u>blow</u> line solution to the stream of primary pulp <u>at or</u> within the intermediate line <u>about three feet of the blow</u> valve;

mixing the intermediate blow line solution and the stream of primary pulp to form a reaction mixture:

discharging the reaction mixture into a retention vessel;

retaining the reaction mixture in the retention vessel to produce a bleached material.

22. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 21, further comprising;

feeding the lignocellulosic material that has been impregnated with the first pretreatment solution for a first reaction time, into a second press;

pressing and discharging the lignocellulosic material from the second press;

impregnating the lignocellulosic material discharged from the second press with a second <u>sodium hydroxide</u> alkaline peroxide pretreatment solution and maintaining the second impregnation for a second reaction time.

- 23. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 21 further comprising adding an <u>a sodium hydroxide</u> alkaline peroxide refiner solution to the lignocellulosic material at the refiner.
 - 24. (Cancelled)
 - 25. (Cancelled)

- 26. (Cancelled)
- 27. (Cancelled)
- 28. (Original) The alkaline peroxide mechanical pulping process of claim 21, wherein the step of feeding the impregnated lignocellulosic material to a refiner having an inlet and a rotating disc within a superatmospheric casing includes maintaining the superatmospheric casing at a pressure of at least about 240kPa.
- 29. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 21, wherein the impregnation solution contains alkali sodium hydroxide, peroxide, and stabilizer; the intermediate blow line solution contains alkali sodium hydroxide, peroxide and stabilizer; and said intermediate blow line solution is at a temperature less than the stream of primary pulp.
- 30. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 22, wherein the first impregnation solution contains by weight per cent 0.3% DTPA; the second impregnation solution contains by weight per cent 0.2% MgSO4, 4.4% silicate, 2.8% TA, and 2.8%H2O2; and the intermediate blow line solution contains by weight per cent 0.16% DTPA, 0.16% MgSO4, 2.3% silicate, 1.8% TA with 0.5% being residual, 2.4% H2O2 with 1.1% being residual.
- 31. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 22, wherein the first impregnation solution contains by weight per cent 0.5% DTPA; the second impregnation solution contains by weight per cent 0.2% DTPA, 0.1% MgSO4, 2.0% silicate, 1.6% TA, and 2.6%H2O2; and the intermediate blow line solution contains by weight per cent 0.13% DTPA, 0.13% MgSO4, 2.5% silicate, 1.2% TA with 0.1% being residual, 2.1% H2O2 with 2.1% being residual.
- 32. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 22, wherein the first impregnation solution contains by weight per cent 0.3%

DTPA, 0.05% MgSO4, 0.7% silicate, 0.2% TA, and 0.5%H2O2; the second impregnation solution contains by weight per cent 0.1% DTPA, 0.08% MgSO4, 1.8% silicate, 1.4% TA, and 1.9%H2O2; and the intermediate blow line solution contains by weight per cent 0.22% DTPA, 0.11% MgSO4, 1.1% silicate, 0.9% TA with 0.2% being residual, 1.2% H2O2 with 1.7% being residual.

- 33. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 22, wherein the first impregnation solution contains by weight per cent 0.4% TA, 0.5% H2O2,0.2% DTPA, 0.04% MgSO4, 0.5% silicate; the second impregnation solution contains by weight per cent 0.14% DTPA, 0.05% MgSO4, 0.5% silicate, 0.4% TA, and 0.6%H2O2; and the intermediate blow line solution contains by weight per cent 0.18% DTPA, 0.06% MgSO4, 1.8% silicate, 1.2% TA with 0.1% being residual, 1.8% H2O2 with 1.1% being residual.
- 34. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 22, wherein the first impregnation solution contains by weight per cent 0.4% TA, 0.6% H2O2,0.18% DTPA, 0.03% MgSO4, 0.3% silicate; the second impregnation solution contains by weight per cent 0.15% DTPA, 0.05% MgSO4, 0.4% silicate, 0.4% TA, and 0.7%H2O2; and the intermediate blow line solution contains by weight per cent 1.7% TA, and 2.8% H2O2 with 1.1% being residual.

35. (Cancelled)

36. (Currently Amended) An alkaline peroxide mechanical pulping process comprising the steps of:

in a primary refiner having a superatmoshperic superatmospheric casing, refining a lignocellulosic material that has been pretreated and impregnated with at least a first sodium hydroxide alkaline peroxide pretreatment solution;

discharging the lignocellulosic material through a blow valve into an intermediate line having at least one solution inlet port;

injecting an sodium hydroxide alkaline peroxide intermediate line solution through

the at least one solution inlet port;

mixing the intermediate line solution and the lignocellulosic material; discharging the lignocellulosic material from the intermediate line; and retaining the discharged lignocellulosic material for a reaction period.

- 37. (Currently Amended) The alkaline peroxide mechanical pulping process of claim 36, wherein the step of refining further includes adding a refiner sodium hydroxide solution of alkaline peroxide at the primary refiner.
- 38. (Original) The alkaline peroxide mechanical pulping process of claim 36, wherein the step of injecting an alkaline peroxide intermediate line solution through the, at least one, solution inlet port and into the intermediate line containing the lignocellulosic material includes injecting an alkaline peroxide intermediate line solution through, at least, one solution inlet port located immediately after a blow valve.
- 39. (Original) The alkaline peroxide mechanical pulping process of claim 36, wherein the step of injecting an alkaline peroxide intermediate line solution through the, at least one, solution inlet port and into the intermediate line containing the lignocellulosic material includes injecting an alkaline peroxide intermediate line solution through, at least, one solution inlet port located immediately prior to a separator.
 - 40. (Cancelled)
 - 41. (Cancelled)
- 42. (Original) An alkaline peroxide mechanical pulping process comprises the steps of:

in a refiner having a casing, additionally refining a lignocellulosic based material that has been previously pretreated and impregnated with at least a first sodium hydroxide alkaline peroxide pretreatment solution and which has been previously refined;

discharging the lignocellulosic based material through a blow valve into an intermediate line having at least one solution inlet port;

injecting an <u>a sodium hydroxide</u> alkaline peroxide intermediate line solution through the at least one solution port;

mixing the intermediate line solution and the lignocellulosic based material; discharging the lignocellulosic based material from the intermediate line; and retaining the discharged lignocellusic based material for a reaction period.

- 43. (Original) The alkaline peroxide mechanical pulping process of claim 42, wherein the refiner casing is superatmospheric.
- 44. (New) The alkaline peroxide mechanical pulping process of claim 1, wherein more than one third of the total sodium hydroxide alkaline peroxide solution added from impregnation to the blow line inclusive, is added at the blow line.
- 45. (New) The alkaline peroxide mechanical pulping process of claim 3, wherein more than one third of the total sodium hydroxide alkaline peroxide solution added from impregnation to the blow line inclusive, is added at the blow line.
- 46. (New) The alkaline peroxide mechanical pulping process of claim 21, wherein more than one third of the total sodium hydroxide alkaline peroxide solution added from impregnation to the blow line inclusive, is added at the blow line.
- 47. (New) The alkaline peroxide mechanical pulping process of claim 23, wherein more than one third of the total sodium hydroxide alkaline peroxide solution added from impregnation to the blow line inclusive, is added at the blow line.
- 48. (New) The alkaline peroxide mechanical pulping process of claim 36, wherein more than one third of the total sodium hydroxide alkaline peroxide solution added from impregnation to the blow line inclusive, is added at the blow line.

49. (New) The alkaline peroxide mechanical pulping process of claim 37, wherein more than one third of the total sodium hydroxide alkaline peroxide solution added from impregnation to the blow line inclusive, is added at the blow line.